

Modeling Aeration in High Pressure Hydraulic Circulation

Bahrom Xaliljonovich Abdullayev, Salimjon Azamdjanovich Rahmankulov
Ferghana Polytechnic Institute, Ferghana, Uzbekistan

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Annotation: The intensity of the pulsation of water flow rates in high-pressure hydraulic units depends on the flow velocity, which leads to the destruction of small waves arising on the free surface. From gravity acting on air bubbles trapped by a stream of water, and on water droplets in the air; from the force of surface tension, preventing the destruction of the free surface of the water; from the hydraulic coarseness of the bubbles (the speed of their rise in calm water) affect the aeration process. The article addresses the above issues.

Keywords: aeration, turbulence scale, averaged speed of high-pressure hydraulic structures, mixing paths.

In many cases, many reservoir hydraulics, for example, in a tubalancom, the reservoir, the condition of air penetration into the flow is not only the yield of turbulent perturbations on the free surface, but also the achievement on the surface surface of approximately 3-4 m / s. The location of turbulent perturbations on the free surface depends on the depth of the stream. The destruction of the waves on the surface of the free surface occurs in the result of the action on them from the air force.

Experiments are shown that the air force is proportional to the square of the flow rate of the flow of relationally air, then, naturally, the criterion of the beginning of aeration must be complex and contain depth and square of water velocity. Therefore, the number of fruits enters most of the proposed criteria for the beginning of aeration.

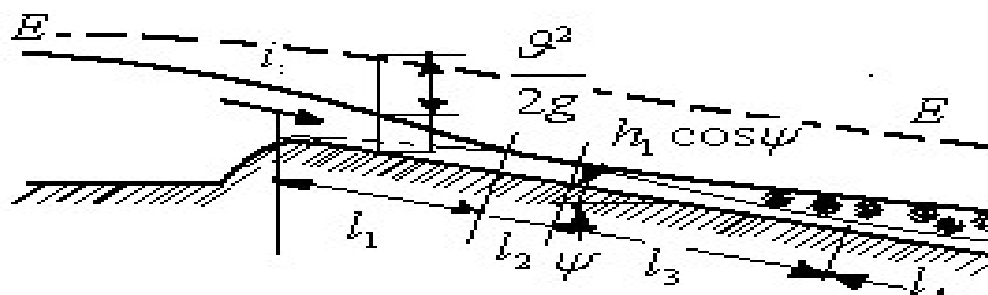


Figure. 1. Replace the flow structure along the length of the speed.

But to reproduce the aeration process on the model, which is notable, is not possible, and the receipt of inventive data is difficult. The intensity of the pulsation of the velocities of the aqueous stream depends on the flow rate, leading to the destruction of small waves arising on the free surface. From the strength of gravity, acting on air bubbles, captured by the flow of water, and on water droplets in the air; from the strength of the surface tension that prevents the destruction of the free surface of the water; From the hydraulic size of bubbles (the speed of their pop-up in calm water) affect the aeration process. And finally, from the perturbation of the free surface by the poor structures and the scientifications of the water. Каждая из выше приведенных сил требуется свой критерий:

$$\text{Frud. } Fr = \frac{g^2}{gl}, \text{ Weber } We = \frac{\rho l g^2}{\nu}, \text{ Reynoldsa } Re = \frac{lg}{\nu}.$$

When modeling on a fruud on the model, in λ If less nature, the strength of gravity acting on air bubble or water drop is less than in kind, in λ^3 once; Power of surface tension - λ , once; The force of friction on which the hydraulic size of the bubble depends, - $\lambda^{\frac{3}{2}}$ times. The kinetic energy of bubbles and drops decreases in λ^4 Once, the work of the forces of surface tension and friction - respectively in λ^2 и $\lambda^{\frac{5}{4}}$ once. This eliminates the possibility of achieving a complete similarity when modeling the capture process of air flow and started aeration. On the model, in λ Once smaller nature, the size of air bubbles and water drops will not be in Once smaller. It is also important to respect the similarity of the relative roughness of the bed.

Studying aeration in laboratory conditions in NIIIVP is produced in trays with a large drop of the levels of the beef, allowing to reproduce the conditions for its occurrence approaching to one-scale.

In [2, 3], on the basis of attentive and extensive laboratory use of aeration (with relative roughness of the tray $\frac{\Delta}{R} = 0; 0,01; 0,02; 0,04; 0,06$ and $0,1$ and meets the beginning of aeration:

$$Fr_{kp} = 45 \left(1 - \frac{\Delta}{R} \right)^{14}$$

Where R - Hydraulic radius of non-aeronautical stream. From (4-6), the critical speed corresponding to the start of aeration can be represented by the following formula: $g_{kp} = 6,7 \sqrt{gR} \left(1 - \frac{\Delta}{R} \right)^7$ (7)

G.P. Skrebkov and V.S. The synecics [4] proceeded from the calculated model,

Presenting air capture by flow as a result of the water droplets in the airspace. The air bubbles captured by the stream saturate the flow at:

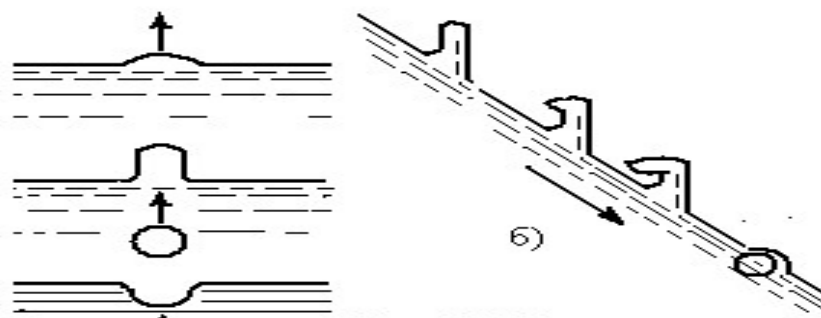


Figure. 2. Mechanism of air cooling accept through free

a) angled air

b) in the breaking of waves

$$\sqrt{\sigma} \phi w \cos \psi \quad (8)$$

Where σ - RMS transverse ripple speed; w - Hydraulic air bubbles, equal to 25 cm / s. The transverse pulsation velocity at the free surface can be expressed through dynamic speed:

$$\sqrt{\sigma} = \beta \sqrt{u_*} = \beta \sqrt{gh_0 \sin \psi}$$

where the coefficient β - according to [66] adopted 0,8; h_0 - Depth of the uniform non-aerated stream; ψ - Angle of inclination of the waterway.

Consequently, inequality (8) can be "represented as:

$$h_0 \sin \psi \phi \frac{w^2}{\beta g} \cos^2 \psi$$

Multiplying the right and left parts of this inequality on C^2 and bearing in mind that when $h_0 \approx Rg = C\sqrt{RI}$ где $I = \sin \psi$, we obtain the formula of the mean velocity at which aeration begins:

$$g_{kp} = \frac{Cw \cos \psi}{\sqrt{0,8g}} \quad (9)$$

or for $w = 0,25 \frac{M}{c}$

$$g_{kp} = 0,089C \cos \psi \quad (10)$$

T. G. Wagoney-Syankhensky [1] proceeded from the formula for the propagation rate of the wave of perturbation on the surface of the water - air of the potential stream. The flow, which shifts on the speed or drainage, can be approximately considered potential, based on the fact that in this case the inertia strength is knowledgeably more resistance forces.

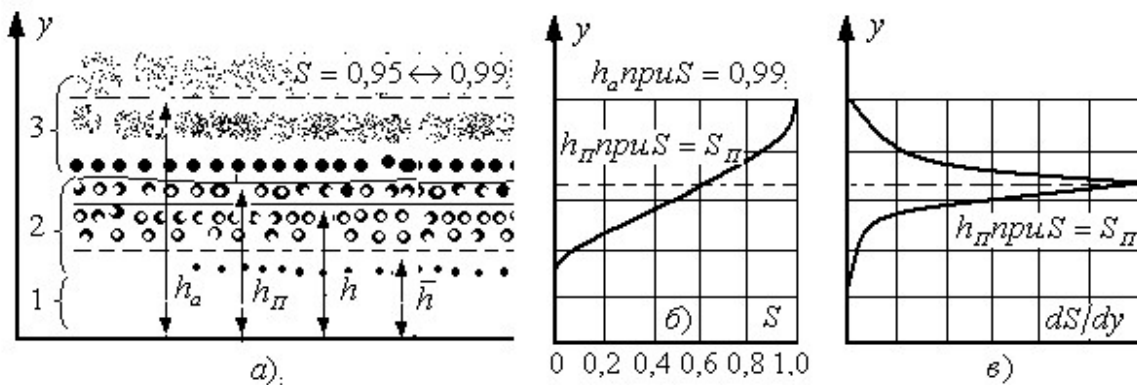


Figure 3. Cheme impexless water flow

(a) and the nature of the distribution of concentration air (b.v)

In the field of gravity, at the rate of water flow, air velocity and the depth of the wave of perturbation on the surface of the section, it is distributed (excluding the effect of surface tension forces) with ambulence (Fig.4.) [46]:

$$c = \frac{\rho u + \rho_a u_a}{\rho + \rho_a} \pm \sqrt{\frac{g\lambda(\rho - \rho_a)}{2\pi(\rho + \rho_a)} \frac{2\pi h}{\lambda} - \frac{\rho \rho_a (u - u_a)^2}{(\rho + \rho_a)^2} \frac{2\pi h}{\lambda}}$$

where ρ, ρ_a - density, respectively water and air; g - acceleration of gravity; λ - wavelength.

insofar as $\rho_a \ll \rho$, namely $\frac{\rho_a}{\rho} \approx \frac{1}{770}$,

That can be considered

$$\frac{(\rho - \rho_a)}{(\rho + \rho_a)} \approx 1 \text{ и } \frac{\rho \cdot \rho_a}{(\rho + \rho_a)^2} \approx \frac{\rho_a}{\rho}.$$

Then for $u \approx u_a$ and oblique bottom of the bed:

$$c = u \pm \sqrt{\frac{g_* \lambda}{2\pi} \frac{2\pi h}{\lambda} - \frac{\rho_a u^2}{\rho} \frac{2\pi h}{\lambda}}$$

where $g_* = g \cos \psi$, ψ - the angle of inclination. For the waves of a small length on the wave propagation rate, in addition to gravity, the forces of the surface tension [50] also have a noticeable effect of [50],

$$\text{which leads to the formula [16]} \quad c = u \pm \sqrt{\frac{g_* \lambda}{2\pi} \frac{2\pi h}{\lambda} + \frac{2\pi \sigma}{\rho \lambda} \frac{2\pi h}{\lambda} - \frac{\rho_a u^2}{\rho} \frac{2\pi h}{\lambda}} \quad (12)$$

σ - поверхностное натяжение жидкости.

Wave propagation rate in fixed liquid ($u = 0$) excluding surface tension and when assumed that $\rho_a = 0$, Determined by the formula:

$$c = \sqrt{\frac{g_* \lambda}{2\pi} \frac{2\pi h}{\lambda}} \quad (13)$$

With an increase in the flow rate to a certain limit value, the conditioned expression of formula (12) becomes negative. This means that the wave motion under consideration is impossible physically: waves are degraded, causing aeration. Thus, the condition of the beginning of aeration is the equality zero of the courted expression of formula (12) or

$$u^2 = \frac{g_* \lambda \rho}{2\pi \rho_a} + \frac{2\pi \sigma}{\lambda \rho_a} \quad (14)$$

To obtain the calculated formula, the wavelength λ in (14) expressed through the length of the mixing path l and then through the hydraulic radius R , And surface speed u - through average speed \mathcal{Q} .

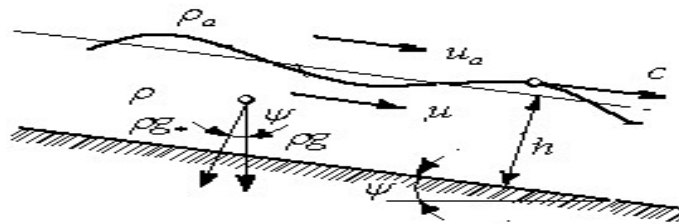


Figure. 4. Inspection of perturbation waves on the surface of the section

One of the values determining the scale of the flow turbulence is determined as it is known, the length of the mixing path l , Equal on L. Prandtl Distance on which the final volumes of liquid (moths) are penetrated in the transverse direction under the influence of velocity ripples. The length of the mixing path, and therefore, the size of the vortex originated at the bottom of the DNA increase in proportion to the distance from the bottom to $l = \chi y$ (χ - constant Pocket). According to the explicit data Nikuraradsis $\chi = 0,36 \leftarrow \rightarrow 0,40$ and constant value χ - saved at distances from the bottom to $y \leq 0,2h$. Vortices reaching a free surface have dimensions $l = \chi h$, where $\chi = 0,36$; wavelength l Determined by the size of the vortices. Because for widespread $R = h$, finally taken into expression (14) $\lambda = 0,36R$.

For transition in expression (14) from surface speed; The logarithmic law of the distribution of the rainy, obtained by the pocket [121, p.546]:

$$\frac{u_{nos} - u}{u_*} = -\frac{1}{\chi} \left\{ \ln \left[1 - \sqrt{\frac{y}{h}} \right] + \sqrt{\frac{y}{h}} \right\} \quad (15)$$

where u_{nos} - Surface speed; u - Local averaged speed at a point immersed on the depth y ; u_* - Dynamic speed. Expressing u_* Through average speed:

$$u_* = \sqrt{gRI} = \frac{\mathcal{G}\sqrt{g}}{C}$$

Formula (15) give the form:

$$\frac{u_{nog}}{\mathcal{G}} = \frac{u}{\mathcal{G}} - \frac{\sqrt{g}}{\chi C} \left\{ \ln \left[1 - \sqrt{\frac{y}{h}} \right] + \sqrt{\frac{y}{h}} \right\} \quad (16)$$

If we take that at a distance from a free surface $\frac{y}{h} = 0,84$ local averaged speed $u = \bar{\mathcal{G}}$, That instead (4-16) we get:

$$\frac{u_{nog}}{\mathcal{G}} = 1 + \frac{\sqrt{g}}{\chi C} \quad (17)$$

Since accepted

$$\ln[1 - \sqrt{0,84}] + \sqrt{0,84} \approx -1.$$

From the power law distribution law in the radius round pipe r_0 :

$$\frac{u}{u_{\max}} = \left(\frac{y}{r_0} \right)^{\frac{1}{n}}$$

[1] when $\frac{1}{n} = \frac{1}{10}$ has a local averaged speed $u = \mathcal{G}$ at a distance from the surface $\frac{y}{h} = 0,763$. With

coefficient of coefficient for manning $C = \frac{1}{n} R^{\frac{1}{6}}$

$$\frac{u_{nog}}{\mathcal{G}} = 1 + \frac{\sqrt{gn}}{\chi R^{\frac{1}{6}}} \quad (18)$$

Substituting in (18) speed u_{nog} no (14) when $\lambda = 0,36R$, separate critical number

frud. $Fr_{kp} = \frac{\mathcal{G}^2}{gR}$, at which aeration begins:

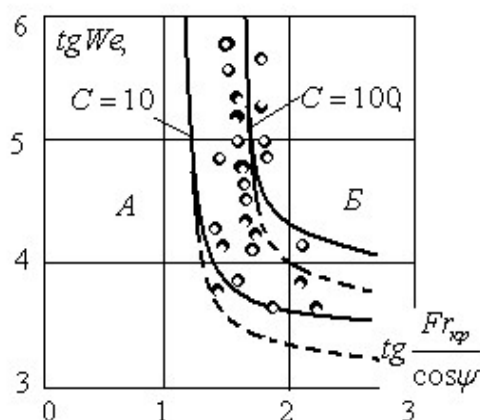
$$Fr_{kp} \geq \frac{\rho\chi}{2\pi\rho_a} \frac{1 + \frac{4\pi^2\sigma}{\rho g_* \chi^2 R^2}}{\left(1 + \frac{n\sqrt{g}}{\chi R^{\frac{1}{6}}} \right)} \cos\psi, \quad (19)$$

when $\sigma = 36 \cdot 10^{-2} \frac{H}{M}$.

$$\vartheta_{kp} = 6,63 \sqrt{gR \cos \psi \left(1 + \frac{0,0011}{R^2} \right)} \left(1 + 8,7 \frac{n}{R^{\frac{1}{6}}} \right)^{-1} \quad (20)$$

Surface tension for distilled water at a temperature of 20 parts equals $72 \cdot 10^{-3} \frac{H}{M}$. If there are organic impurities in water σ decreases, however, the decrease σ до $36 \cdot 10^{-3} \frac{H}{M}$ It should be considered as an empirical directing, increasing calculation accuracy ϑ_{kp} . Aeratorial criteria is given to mind:

$$\frac{Fr_{kp}}{\cos \psi} = \frac{44}{\left(1 + \frac{8,7}{C} \right)^2 - \frac{13300}{We}} \quad (21)$$



Rice. 5. Effect of surface tension Number of Weber WE on the number of FRU Yes FR corresponding to the beginning of the aratration

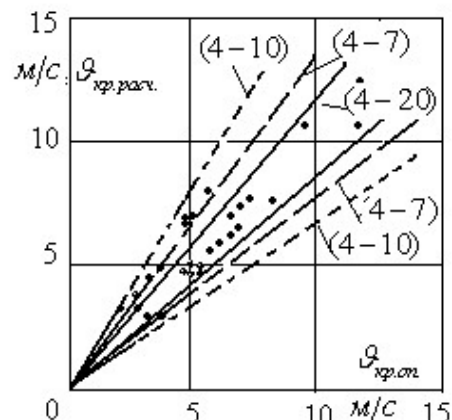


Fig.6. Radiatric rejection of settlement values of the speed of starting ariality of experimental data. Fativity

This expression allows you to identify the effect of surface tension on the occurrence of aeration, i.e., the number of Web $We = \frac{\rho R \vartheta^2}{\sigma}$, expressing the relationship of the power of inertia to the forces of surface tension. In Fig. 5. The expression (21) is presented in the form of a graph, the meaning of which is as follows. In the area of A when $\lg Fr \pi 1$

($Fr = 10$) and any values $\lg We$, as well as $\lg Fr \phi 1$ и $\lg We \pi 3,5$ Aeration does not occur. It occurs at $\lg Fr \phi 1$ и $\lg We \phi 3,5$. And always takes place in the region B.

Fig. 6. The comparison of the experimental speed data is given. g_{kp} with calculated and shown borders corresponding to the standard deviations of settlement values g_{kp} from observed (in percent). The standard deviation of the software (20) was 15%, according to (7) - 22%, software (10) - 39.9%.

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